

NO_x Control & Measurement Technology for Heavy-Duty Diesel Engines

W.P. Partridge, J.A. Pihl
Oak Ridge National Laboratory

S. Joshi, N. Currier, R. Daya, K. Kamasamudram, A. Yezerets

Cummins Inc.

H. Hess, H.-Y. Chen **Johnson Matthey Inc.**

DOE Vehicle Technologies Office Annual Merit Review & Peer Evaluation Meeting June 13, 2019; Arlington, VA

VTO Program Managers: Gurpreet Singh & Ken Howden







Overview

Timeline

- New Project
 - 2018 VTO AOP Lab Call
 - AOI-1E: Low Temperature
 Emissions Control (Heavy Duty)
- Year 1 of 3-year
 - Start Date: Oct. 1, 2018
 - End Date: Sept. 30, 2021
 - Percent Complete: 16%

Budget

- 1:1 DOE:Cummins cost share
- FY19 DOE Funding: \$450k
 - DOE share: \$450k
 - Cummins share: \$450k (in kind)

Barriers

- From **21**st **CTP Research Blueprint**:
 - Emission control cost
 - Low-temperature emission control
 - Robustness in real-world application
- From U.S. DRIVE Roadmap:
 - Low-temperature emission control
 - Compliance via Real Driving Emissions (RDE)
 - Emissions control durability

<u>Partners</u>

- ORNL & Cummins Inc.
- Johnson Matthey (participant)



Milestones

FY	Qtr	Milestone & Objectives	Status
2018	4	Experimentally characterize reaction steps for a commercial SCR catalyst, over a conditions relevant to model development	complete
2019	2	Outline structure for half-cycle-based model	complete
2019	3	Protocol experiments on degreened commercial catalyst	on track



Responses to 2018 Review Comments (Previous Project)

- Desire to have more project participants
 - Catalyst supplier formally incorporated as a participant
 - Beyond their traditional contributions via the separate CMI-JMI partnership
- Integrate kinetic model with a thermal model
 - Cummins' In-House Detailed Model contains kinetics and heat transfer



Collaborations and Coordination

ORNL: Bill Partridge

Cummins: Saurabh Joshi



Johnson Matthey: Howard Hess

Formally included in CRADA and Project documentation

Teamwork & Roles

ORNL • Diagnostics • Measurements	<u>Cummins</u>ModelingField ageing	Johnson MattheyModel catalyst samples					
<u>Joint</u> PlanningResults interpretationMonthly+ telecons							





- Interactions with technical community
 - 1 archival publication
 W.P. Partridge, S.Y Joshi, J.A. Pihl, N.W. Currier (2018). "New Operando Method for Quantifying the Relative Half-Cycle Rates of the NO SCR Redox Cycle Over Cu-Exchanged Zeolites," Applied Catalysis B: Environmental, 236, 195-204. doi.org/10.1016/j.apcatb.2018.04.071
 - 1 invited book chapter
 - 3 presentations (1 invited)





Key Challenge Addressed by Project

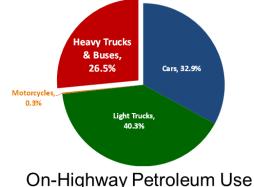
- Efficient catalyst performance under Field-Aged & Low-Temperature conditions
 - How does field ageing impact SCR reaction network
 - Mechanistic impact of 'low-temperature' SCR formulations
 - Improve catalyst durability under Real-World Driving Conditions

Relevance

- Durability advances critical to meeting increasing manufacturer warranty requirements
 - Useful Life: compliance on certification drive cycle
 - Warranty: compliance under real-world-driving conditions
 - E.g., Lower temperatures, higher space velocities, & other real-driving 'off-cycle' conditions
- Better catalyst performance allows engine to be optimized for fuel efficiency

Heavy Heavy Duty Emissions Regulations							
Curr	ent	2022	Projected '26/'27				
CARB/EPA	CARB						
Useful Life (miles)	Warranty (miles)	Warranty (miles)	Useful Life (miles)	Warranty (miles)			
435,000 (10yr, 22k hr)	100,000 (5yr, 3k hr)	350,000 (5yr)	1,200,000	800,000			

Rapidly Increasing Warranty & Useful-Life Demands



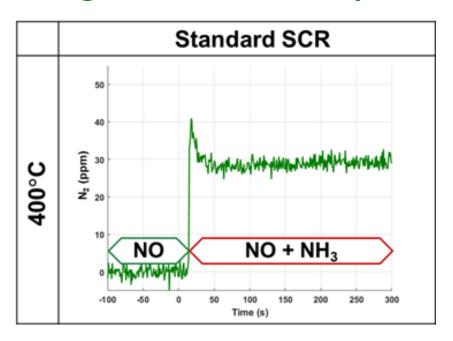
On-Highway Petroleum Use (Source: Transportation Energy Data Book)

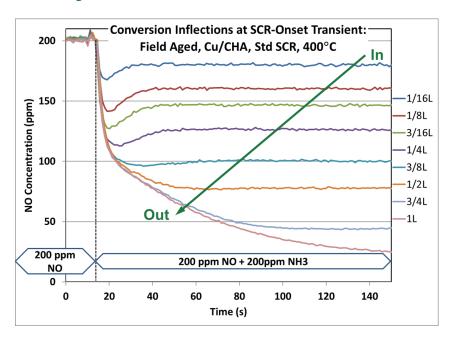






Using Transients to Improve Catalyst Performance





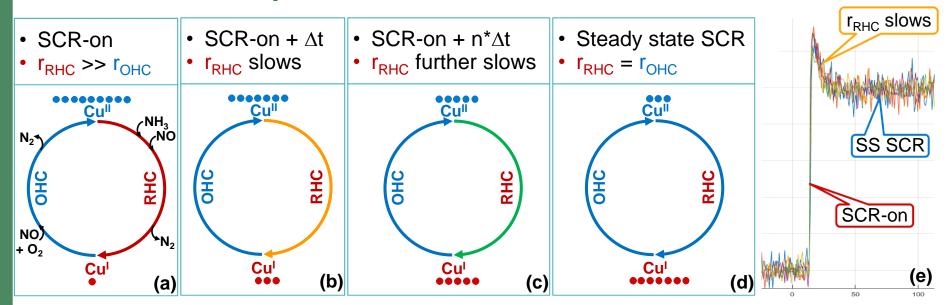
- Conversion Inflections (CI) can occur with Cu/SCR catalysts at SCR onset
 - Fast conversion onset & Slower conversion degradation to steady state level
- Cl nature varies catalyst conditions
 - SCR type and temperature
 - Catalyst location (local concentrations and space velocity)
 - Catalyst age
- Transient CI can be used to understand kinetic origins of catalyst performance







CI Transient Shape Reflects SCR Kinetic Parameters



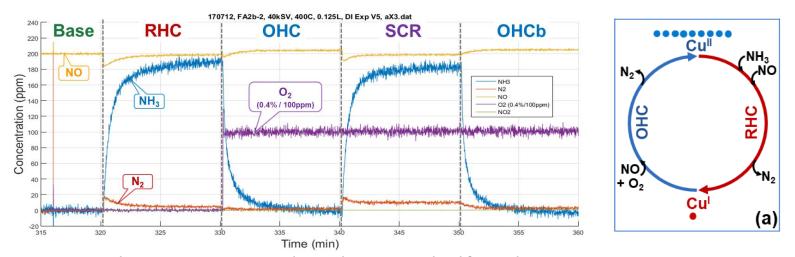
- Cu SCR can be viewed as cyclic Cu reduction and oxidation
 - RHC: Reduction Half Cycle oxidized Cu (Cu^{II}) is reduced to Cu^I
 - OHC: Oxidation Half Cycle Cul is reoxidized to Cull completing the cycle
- Half-cycle rate imbalances induce CI at SCR onset
 - CI occurs when the RHC rate is faster than the OHC rate; $r_{RHC} > r_{OHC}$
 - r_{RHC} progressively slows to match r_{OHC} at steady state
- Detailed CI Shape depends on half-cycle kinetic parameters
 - Use to study kinetic impact of catalyst ageing & formulation



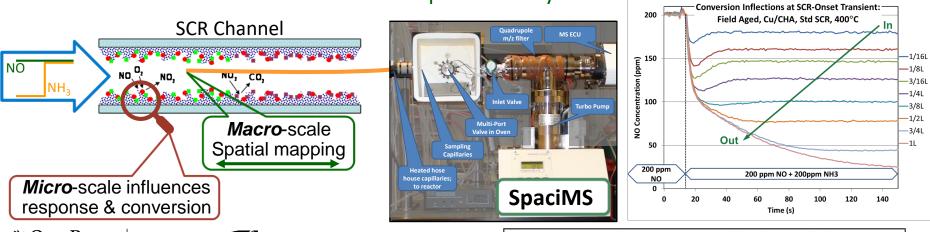




CI Transient Response can be Measured for Each Half Cycle



- Experimental 5-Step protocol probes SCR half-cycle components
- SpaciMS allows for spatial mapping of CI transients
 - Evolution of CI transient
 - Variations with concentrations & space velocity







Cu-Redox Model Shows CI Varies with Kinetic Parameters

Standard SCR

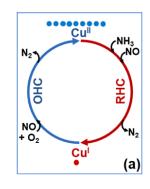
RHC:
$$Cu^{II}(OH)(NH_3) + 2 \cdot NH_3 + NO \rightarrow Cu^{II}(NH_3)_2 + N_2 + 2H_2O$$

$$r_{RHC} = k_{RHC} \cdot [Cu^{II}] \cdot [NO] \cdot (\theta_{NH3})^{\sim 0} \cong k_{RHC} \cdot [Cu^{II}] \cdot [NO]$$

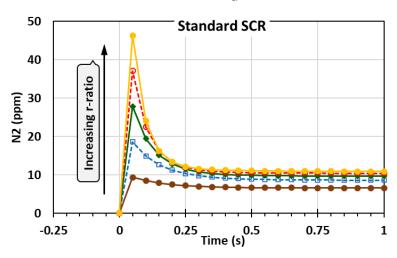
$$OHC: 2 \cdot Cu^{II}(NH_3)_2 + O_2 + 2 \cdot NO \rightarrow 2 \cdot Cu^{II}(OH)(NH_3) + 2 \cdot N_2 + 2 \cdot H_2O$$

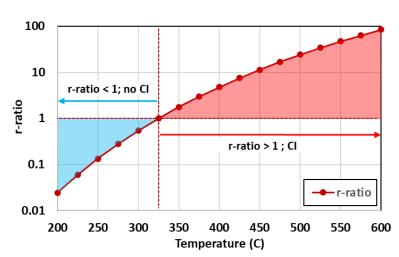
$$r_{OHC} = k_{OHC} \cdot [Cu^{II}]^2 \cdot [O_2] \cdot [NO]$$

$$Net Standard SCR: 4 \cdot NO + 4 \cdot NH_3 + O_2 \rightarrow 4 \cdot N_2 + 6 \cdot H_2O$$



- Half-cycle models formulated for Standard & Fast SCR
 - Correct formulation & kinetic parameter set will accurately predict CI transient
- Predicted CI more distinct with increasing r-ratio & Temperature (r-ratio = r_{RHC} / r_{OHC})
 - Influence of specific E_a & A factors for RHC & OHC ($k = A e^{-Ea/RT}$)



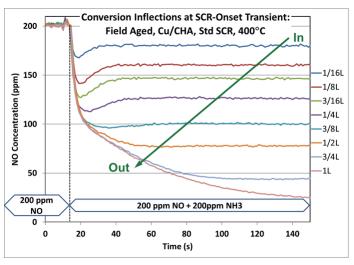


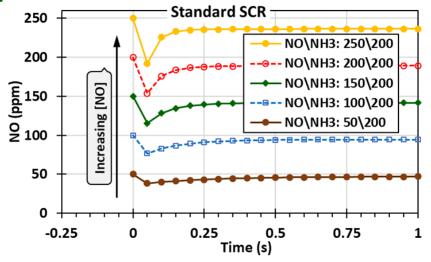






Cu-Redox Model Predicts Experimentally Observed Trends



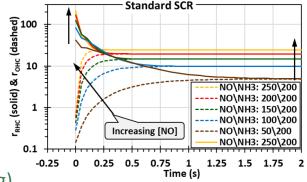


NO CI trends consistent with measured trends along catalyst axis

- Greatest CI at catalyst front (where NO is high)
- CI degrades along catalyst as NO-conversion progresses



- More distinct CI at higher temperatures
- RHC & OHC rates converge at SS (mainly due to RHC slowing)



- Cu-Redox model accurately describes transient CI nature
- Spatiotemporal measurements may be used to tune a kinetic model



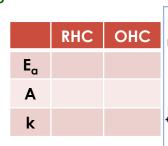


Technical Approach

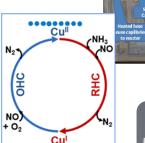
- 1. Use Transient-Response Method to determine SCR kinetic parameters
- 2. Measure CI transient shapes
 - 5-Step Protocol & spatiotemporal mapping



Using data & Cu-redox model



SCR Channel





- 4. Baseline DeGreened catalyst kinetic parameters
 - Steps 2 & 3
- 5. Study how *Field Ageing* impacts kinetic parameters
 - RHC & OHC specific impacts vs. DeG values
 - Pathways to improved durability and control
- 6. Study how Catalyst Formulation impacts kinetic parameters
 - Mechanistic origin of formulation benefits
 - Pathways to improved low-temperature aged performance



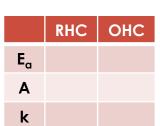


FY2019 Activities and Plans

- Measure CI for new state-of-the-art Commercial Cu-SSZ-13 SCR
 - DeGreened & Standard SCR conditions
 - 5-Step Protocol; Spatial & temperature sweeps



- Validate Cummins' In-House detailed model at higher local space velocities
 - AVL Boost; includes transport, kinetics, heat transfer
- Develop detailed half-cycle Cu-oxidation-state model (using AVL Boost)
 - Beyond conceptual and simple kinetic model of previous project
 - Use to fit Cu-redox half-cycle kinetic parameters



- Fit half-cycle kinetic parameters
 - DeGreened Cu-SSZ-13 in Standard SCR
 - RHC & OHC parameters

Proof and refinement Pulsed-Response Expe	erimental-Modeling method

- - Use in FY20 & 21 to quantify kinetic-parameter changes
 - Fundamental insights into field-ageing & formulation

Any proposed future work is subject to change based on funding levels







Detailed

Model

(a)

Remaining Challenges & Future Work Key Challenge:

- Efficient catalyst performance under Field-Aged & Low-Temperature conditions
 - Mechanistic insights of how Ageing & Formulation impact SCR performance
 - Improved catalyst durability under Real-World Driving Conditions

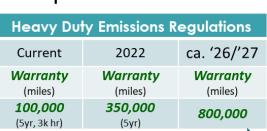
Future Work:

- FY20: Kinetic study of Formulation & Field Ageing impacts
 - How Field Ageing impacts RHC & OHC vs DeG baseline Cu-SSZ-13
 - SCR-specific improvement concepts (e.g., dosing, formulation)
 - System-level improvement concepts (e.g., upstream oxidation catalyst)
 - Kinetic origins of *Low-Temperature-Formulation* benefits
 - Understanding performance benefits in the context of kinetic changes
 - · Pathways for next-level formulation tuning



- Kinetic analysis of next-level low-temperature formulations
- Assess pathways to improved catalyst durability
 - Using Cu-redox integrated into In-House model
- Methods for catalyst-state assessment and control

Any proposed future work is subject to change based on funding levels



RHC

OHC

Solution Pathway







Summary

Relevance

- Focus is on kinetic origin of low-temperature performance and field aged SCR catalysts
- Project work enables improved catalyst knowledge, models, design, OBD & control
- Advances DOE goals for improved fuel economy, durability, & real-world emissions

Approach

- Apply experimental protocol to probe transient response of Cu-redox half-cycle steps
- Develop and apply model to fit Cu-redox half-cycle kinetic parameters
- Study kinetic impacts of low-temperature formulations and field-aged catalysts

Technical Accomplishments

- New project and CRADA established
- Catalyst supplier, Johnson Matthey, incorporated into project as participant
- FY19 plan to demonstrate pulsed-response method of determining kinetic parameters

Collaborations

- Johnson Matthey incorporated as project and CRADA participant
- Communicate with community via presentations & publications
- Future Work (Any proposed future work is subject to change based on funding levels)
 - Determine kinetic origins of performance for low-temperature formulations
 - Determine impact of field-ageing on kinetics of commercial Cu-SSZ-13 SCR catalyst

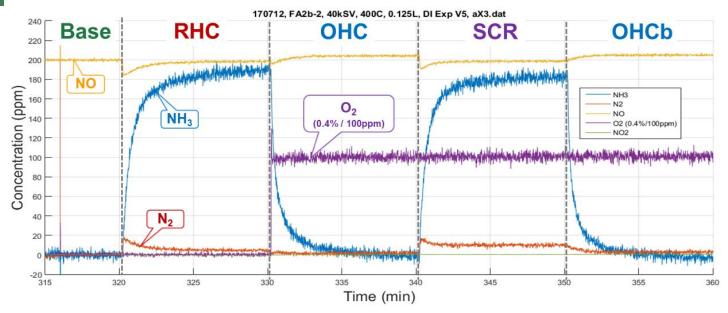




Technical Back-Up Slides



5-Step Experimental Protocol for Studying Onset Transients



- Individual RHC, OHC & SCR transitions investigated
 - Step 1 Base: $5\% H_2O + 200$ ppm NO_x in Ar
 - Step 2 RHC: Base + 200ppm NH₃
 - Step 3 OHC: Base + 0.4% O₂
 - Step 4 SCR: Base + O₂ + 200ppm NH₃
 - Step 5 OHCb: Base + O₂
- Different SCR mixtures investigated
 - Standard, Fast & NO₂
 - -200ppm NO_x

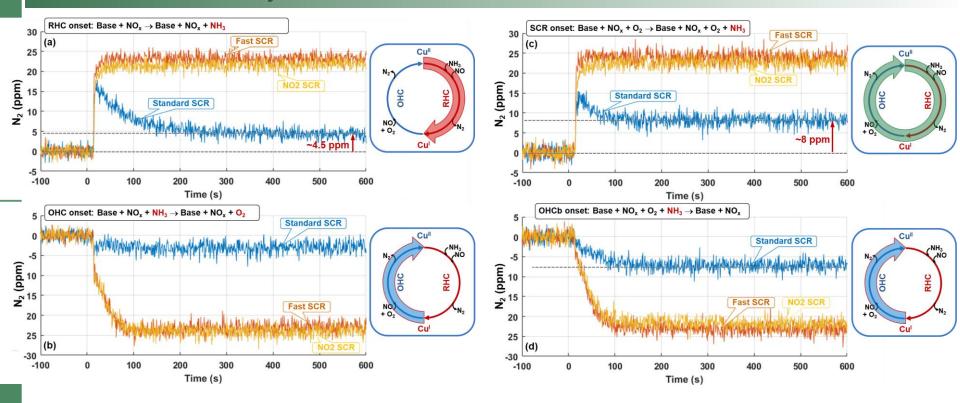
- Commercial SCR
- Field Aged: FA-2b
- 400°C
- 1/8L
- 40k SV





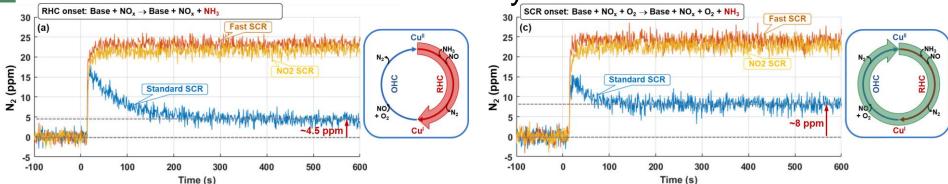


Measured Half-Cycle Onset Transients





Measurements of Individual Half-Cycle Onset Transients

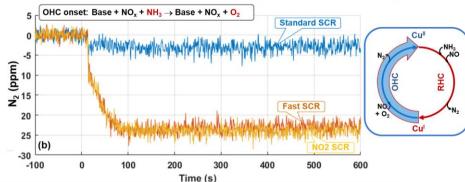


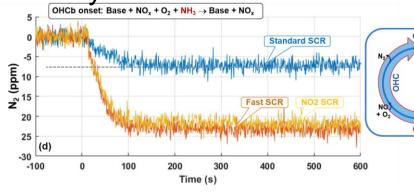
- 5-Step Experimental Protocol designed to study half-cycle onset transients & CI
 - Allows individual and combined half cycles to be probed (see Tech. Backup Slides)
- Standard SCR Onset Transients
 - RHC onset shows CI
 - Initial fast step-like transients indicates native RHC rate
 - Conversion degrades over ~200s as Cu^{II} is depleted
 - Non-zero SS due to contaminant or bulk oxygen driving OHC
 - For SCR onset
 - CI is smaller & faster, and SS conversion is greater
 - both half-cycles are active
- NO₂ & Fast SCR Onset Transients
 - Identical, fast, step-like transients without CI
 - Suggests OHC occurring via NO₂, and O₂ not participating
- OHC transients offer additional insights (see Tech. Backup Slides)





Measurements of Individual OHC Half-Cycle Onset Transients





OHC Onset Transients

- Starts from maximum [Cul] following RHC step
 - [Cu^I] greater than at OHCb start
 - Causes greater step-like onset vs. OHCb transient
- NO₂ & Fast SCR transient are identical
 - Initially step-like, then slow over ~100s as Cu^I is depleted
- Standard SCR show NO CI (see 5-Step Protocol figure)
 - Signal-to-noise is too small to resolve similar N2 CI

OHCb Onset Transients

- These follow SCR, and thus start from lower [Cul] initial condition
- Slower Standard SCR transient (~150s) vs. NO₂ & Fast SCR (~100s)
 - Different OHC mechanism & kinetics for O₂- vs NO₂-driven OHC
- NO₂ & Fast SCR transients are identical as with OHC
 - Suggests OHC driven by NO₂, and O₂ is practically inert





Half-Cycle based Model for Standard & Fast SCR

Standard SCR

RHC:
$$Cu^{II}(OH)(NH_3) + 2 \cdot NH_3 + NO \rightarrow Cu^{I}(NH_3)_2 + N_2 + 2H_2O$$
 (1)

$$r_{RHC} = k_{RHC} \cdot [Cu^{II}] \cdot [NO] \cdot (\theta_{NH3})^{\sim 0} \cong k_{RHC} \cdot [Cu^{II}] \cdot [NO]$$
(2)

OHC:
$$2 \cdot \text{Cu}^{\text{I}}(\text{NH}_3)_2 + \text{O}_2 + 2 \cdot \text{NO} \rightarrow 2 \cdot \text{Cu}^{\text{II}}(\text{OH})(\text{NH}_3) + 2 \cdot \text{N}_2 + 2 \cdot \text{H}_2\text{O}$$
 (3)

$$r_{OHC} = k_{OHC} \cdot [Cu^{l}]^{2} \cdot [O_{2}] \cdot [NO]$$
(4)

Net Standard SCR:
$$4 \cdot NO + 4 \cdot NH_3 + O_2 \rightarrow 4 \cdot N_2 + 6 \cdot H_2O$$
 (5)

Fast SCR

RHC:
$$Cu^{II}(OH)(NH_3) + 2 \cdot NH_3 + NO \rightarrow Cu^{I}(NH_3)_2 + N_2 + 2H_2O$$
 (1)

$$r_{RHC} = k_{RHC} \cdot [Cu^{II}] \cdot [NO] \cdot (\theta_{NH3})^{\sim 0} \cong k_{RHC} \cdot [Cu^{II}] \cdot [NO]$$
 (2)

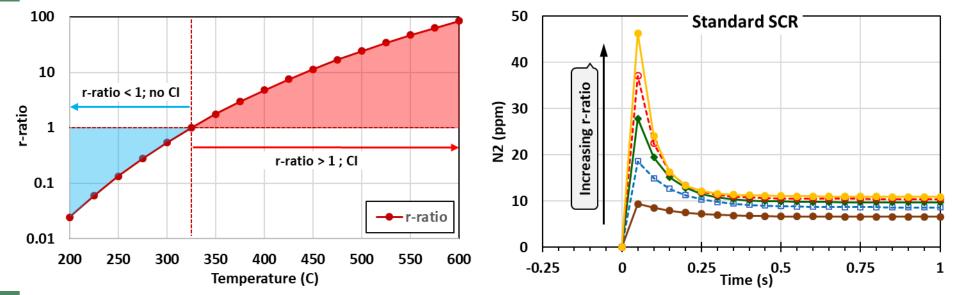
OHC:
$$Cu^{I}(NH_{3})_{2} + NO_{2} \rightarrow Cu^{II}(OH)(NH_{3}) + N_{2} + H_{2}O$$
 (6)

$$r_{OHC} = k_{OHC} \cdot [Cu^{l}] \cdot [NO_{2}]$$
 (7)

Net Fast SCR:
$$2 \cdot NO + 2 \cdot NO_2 + 4 \cdot NH_3 \rightarrow 4 \cdot N_2 + 6 \cdot H_2O$$
 (8)



Global Model Predicts Consistent Cl Nature & Trends

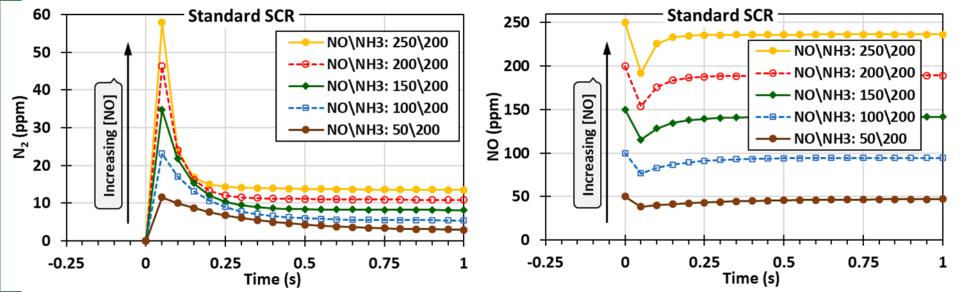


- Half-cycle model exercised to study how kinetic parameters influence CI
 - Model details shown in Tech. Backup Slides
- Ratio of half-cycle rates (r-ratio = r_{RHC} / r_{OHC}) increases with temperature
 - CI should be observed when r-ratio > unity
 - Unity crossing point tuned with RHC & OHC pre-exponential factors
- CI becomes more distinct with increasing r-ratio
 - Taller peak, faster tail
 - SS conversion increases with r-ratio
 - Temperature trend is consistent with experimental observations
- CI nature varies with half-cycle kinetic parameters





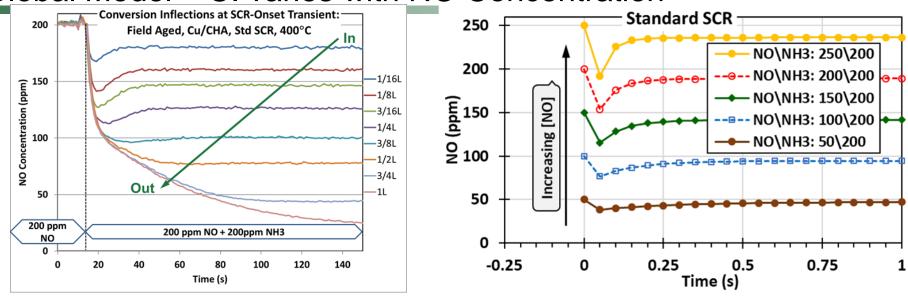
Global Model – CI varies with NO Concentration



- Varying [NO] at constant 200ppm NH₃
 - Cl independent of [NH₃], (zeroth order in [NH₃], see Tech. Backup Slides)
- CI becomes increasingly distinct with increasing [NO]
 - Similar for both N₂ & NO CI



Global Model – CI varies with NO Concentration

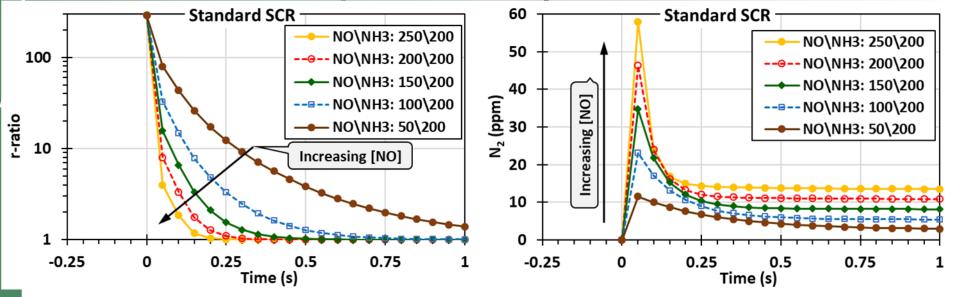


- Varying [NO] at constant 200ppm NH₃
 - Cl independent of [NH₃], (zeroth order in [NH₃], see Tech. Backup Slides)
- CI becomes increasingly distinct with increasing [NO]
 - Similar for both N₂ & NO CI
- NO CI trends consistent with measured trends along catalyst axis
 - Greatest CI at catalyst front
 - CI degrades along catalyst as NO-conversion progresses
- Spatiotemporal measurements may be used to tune a global model
 - Determine half-cycle kinetic parameters from fitting model to measurement data





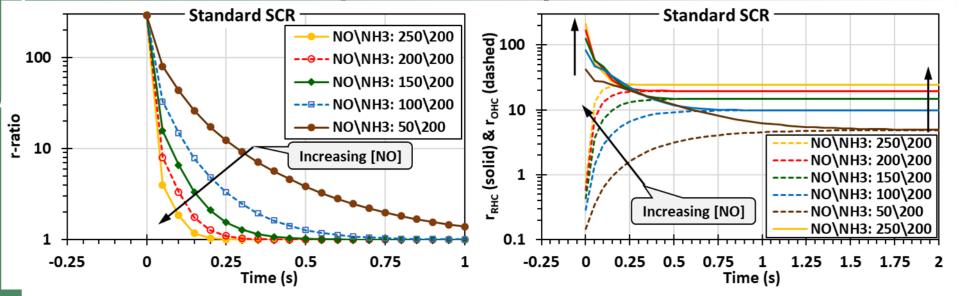
Global Model – Half-Cycle Rates vary with NO Concentration



- r-ratio transient becomes faster with increasing [NO]
 - Distinct CI needs <u>both</u> r-ratio>1 <u>and</u> fast r-ratio transient



Global Model – Half-Cycle Rates vary with NO Concentration

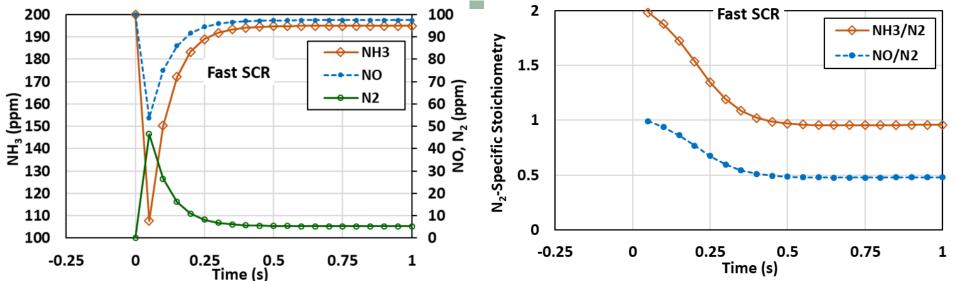


- r-ratio transient becomes faster with increasing [NO]
 - Distinct CI needs <u>both</u> r-ratio>1 <u>and</u> fast r-ratio transient
- RHC & OHC rates converge at steady state
 - Mainly due to RHC slowing
 - Relatively small r_{OHC} increase associated with increasing Cu^I
 - Greater SS conversion & rates with increasing [NO] (consistent with SpaciMS)
 - Rate transient is greater when initial difference is greater
 - Half-cycle rate behavior is consistent with conceptual model
- Model-based studies help advance CI understanding and nature





Global Model – Stoichiometry Varies Through CI Transient



- Model predicts CI for NO, NH₃ and N₂
- CI leading edge reflects RHC stoichiometry

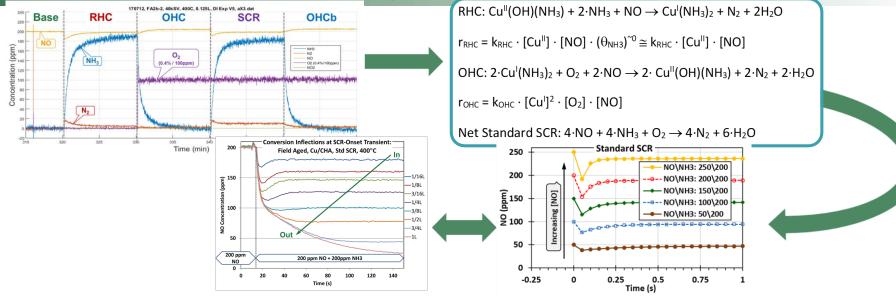
- RHC:
$$Cu^{II}(OH)(NH_3) + 2 \cdot NH_3 + NO \rightarrow Cu^{I}(NH_3)_2 + N_2 + 2H_2O$$

- Steady state reflects Net Fast SCR stoichiometry
 - Net Fast SCR: $2 \cdot NO + 2 \cdot NO_2 + 4 \cdot NH_3 \rightarrow 4 \cdot N_2 + 6 \cdot H_2O$
- Stoichiometry transient reflects half-cycle balancing
 - As rates converge impact of the individual half cycles balance
- Generally similar results for Standard SCR (see Tech. Backup Slides)
- Technique can be use to validate model formulation





Methodology for Formulating & Validating SCR Redox Model

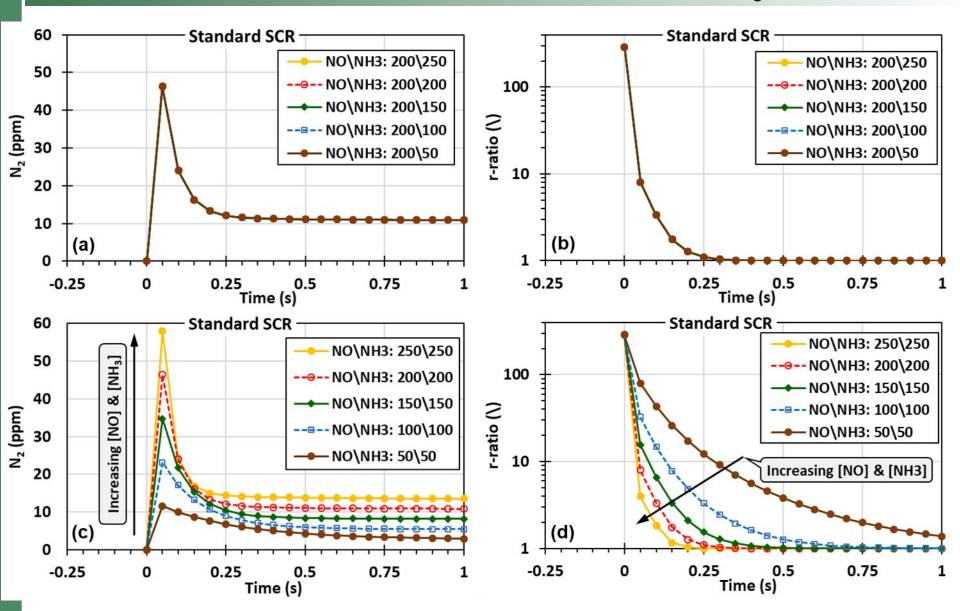


- Step-response experiments to characterize CI & onset transients
 - Range of temperatures and concentrations
 - 5-Step Protocol to investigate individual & combined half cycles
 - Our measurements are the first to resolve half-cycle rate balancing
- Formulate global SCR model based on the two half cycles
 - CI & transient nature varies with model formulation & kinetic parameters
 - Examples show broad dependence of transient performance on model parameters
 - Model CI trends are consistent with measurements
 - Our half-cycle model is the first to show this transient SCR nature
- Use data to formulate, tune & validate the global SCR model Next Steps





Global Model – CI varies with [NO] but not with [NH₃]







Global Model – Stoichiometry Varies Through CI Transient

